

During the relaxation period, because no current is flowing, only diffusion processes will be occurring. The internal resistance of a cell or battery was defined as: $R_{int,i} = (V_o - V_d)_i / I_i$ and the power from the internal resistance as: $P_{int,i} = (V_o - V_d)_i \times I_i$ where $I_i = V_{d,i}/R$ or $I = \text{constant}$ and $i = 1 \dots n$, $V_{o,o} > V_{d,i} > V_{d,n} \geq V_{o,o}/2$.

Directly and integration by parts of internal energy losses lead to the differential equation: $dt/t = b \cdot dP_{int}/P_{int}$, that is, time against power relationship.

Thermodynamically, the calculation was: (1) $V_{o,i} = (V_d + P_{int}/V_d)_i$, where $P_{int,i} = (t_i/a_i)^{1/b_i}$. Using experimentally observed kinetics and the known discharge curve: $(V_{d,i} \text{ versus } t_i, \text{ where } i = 1 \dots n)$ and (2), $dP_{int} = d\{(V_o - V_d) \cdot I\}$, a time-independent differential equation is obtained, which can be integrated as a Clairaut's one.

By short-term discharging, that is: $V_{o,o} > V_{d,i} > V_{d,k}, i = 1 \dots k, k \ll n, V_{d,n} \geq V_{o,o}/2$ and $\phi < t_i < t_k \ll t_n$, and measuring $V_{o,o}$ and $V_{o,k}$ by using time-dependent thermodynamic calculations ($V_{o,i}$ versus $V_{d,i}$) and $dt/t = b \cdot dP_{int}/P_{int}$ the calculated discharge curve: $V_{d,i}$ versus $t_i, i = 1 \dots n, V_o > V_{d,i} > V_{o,n} \gg V_{o,o}/2$ was obtained. The short-time interval, $i = 1 \dots k$, must be divided into: (1) initial conditions: $V_{o,o}, V_{d,1}, V_{d,2}$ versus ϕ, t_1, t_2 , respectively and (2) the control sub-interval: $V_{d,3 \dots k}$ versus $t_{3 \dots k}$ and $V_{o,k}$ measured after a relaxation period. Measured $V_{o,o}$ and $V_{o,k}$ and estimated $V_{o,1}$ values define the $V_{o,n}$.

The above equations were verified by experiment and published discharge data on primary and secondary cells and batteries, ranging in size from small to stationary designs as large as 1000 Ah, with voltage strings as high as 380 V.

By the calculated discharge curve, using known thermodynamic and kinetic data, a primary or secondary cell or battery may be investigated as an electrochemical system.

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New achievements in the cycle life of the silver/zinc battery

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Shape-change and dendritic growth are the main drawbacks limiting the cycle life of the silver/zinc battery. These problems can be overcome by insertion of thin high-porous nickel membranes between the electrodes of the battery. In this poster are presented experimental data on the performance of silver/zinc batteries containing these membranes and results of cycling tests. The results reveal a substantial increase of the cycle life of the silver/zinc battery without any significant effect of the membranes on its performance.

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Development of cell components for a 20 Ah, 12 V secondary zinc/air battery

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Electrically rechargeable zinc/air-batteries are being considered for both electric vehicle and portable device applications. The high theoretical (1150 Wh kg^{-1}) as well as practical specific energy ($60 \text{--} 150 \text{ Wh kg}^{-1}$) are major advantages of the secondary zinc/oxygen battery. The low cost and low toxicity of the materials involved are also an important factor.

By developing a durable perovskite-catalyzed bifunctional oxygen electrode and a long-lived pasted zinc electrode, the cycle life behaviour of secondary zinc/oxygen cells has been improved considerably [1].

The tested monopolar cells consisted of one pasted zinc electrode, having a nominal capacity of 2.5 Ah and an electrode size of 25 cm^2 sandwiched between two bifunctional oxygen electrodes.

In this poster we will present the scale-up of the manufacturing method for the pasted zinc electrodes as well as for the bifunctional oxygen electrodes. The electrode size was increased from 25 to $150 \text{--} 200 \text{ cm}^2$. Moreover, results obtained with larger zinc/oxygen batteries having a monopolar electrode arrangement will be presented. Cycle life, discharge capacity, specific power and specific energy data of the tested batteries will be shown in relation to the results obtained with single (2.5 Ah) cells.

References

- [1] S. Müller, F. Holzer, C. Schlatter, C. Comninellis and O. Haas, *Proc. of the Rechargeable Zinc Batteries Symposium, 188th Meeting of the Electrochem. Soc., Chicago, Oct. 1995*.

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Glassy carbon capacitor stack

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To meet the peak power demands in electric or hybrid vehicles, great efforts are being made to develop high power density, high energy density capacitors, such as electrochemical double-layer capacitors (EDC). The energy storage arises from the double-layer formed at the interface between electrolyte and electrode. Low internal resistance of the capacitor is required to reach high power.